Focused Cross Flow LBE Target for ESS

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2003 reference design for a mercury target
- concept
- boundary conditions
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- proton energy and beam profile
- pulse frequency
- short pulse $\Rightarrow$ long pulse

Focused Cross Flow Target
- concept
- updated boundary conditions
- pros and cons

Conclusions and outlook
2003 reference design for a mercury target

- **concept**

- **Outlet duct**

- **Inlet ducts**

- **Proton beam**

1: proton beam entry window;
2: bottom flow separator plate with potentially needed gas injector system;
3: lateral flow separator plate;
4: indicated mercury center flow;
5: indicated mercury lateral flow.
2003 reference design for a mercury target

boundary conditions

- 5 MW beam power / ~2.9 MW heat deposition (incl. 20% safety margin)
- 50 Hz pulse frequency
- 1.4 μs pulse length
- 1.334 GeV proton energy
- elliptical beam footprint (200mm x 60mm)
- parabolic beam profile
- 175 kg/s mercury flow
  (best operating conditions for 15\% of total mass flow rate through bottom inlet duct)
- 100 °C inlet temperature
- ~220 °C mean outlet temperature

  - $$\Delta T_{\text{window}} \approx 7 \text{ K / pulse}$$
  - $$\Delta T_{\text{Hg}} \approx 37 \text{ K / pulse}$$
2003 reference design for a mercury target

- new findings

- flow instabilities (transient effects and effects due to slightly unsymmetric inlet conditions) can lead to zones of high temperatures in the bulk outlet region of the target, alternately touching the walls

left: stationary calculation performed for a half-model showing stable vortices in the front part

right: transient calculation performed for a full-model showing strong fluctuations
2003 reference design for a mercury target

new findings

left: transient calculation for perfectly symmetric inlet conditions

right: transient calculation for unsymmetric inlet conditions (mass flow rate suddenly increased by 2% for right and decreased by 2% for the left side duct)
2003 reference design for a mercury target

new findings

- time scale of the long-pulse (2 ms) is still small compared to inertia effects of the target material in the rear end of the target
- thermal expansion of the target material is compensated by local compression of the material itself and a local expansion of the target container in the front part
- expansion of target container may lead to significant stresses in the window region

Stressing of the target window for a mercury long-pulse target at 16 $\frac{2}{3}$ Hz
Changes to boundary conditions

LBE as preferred liquid metal

- LBE as preferred target material for a liquid metal target
  - same pressure drop can be expected for a mass flow rate of:
  - heat removal capability is comparable:
  - heat transfer coefficients are comparable:
    (e.g. formulas for turbulent pipe flow, \( d \approx 100\text{mm} \)):
  - thermal-hydraulic design is similar for mercury and LBE

but

- to avoid solidification of LBE, the inlet temperature must be significantly higher: 175 – 200°C (> 125°C) for LBE instead of 100°C for mercury
- no risk of evaporation (evaporation temperature is 1670°C for LBE instead of 357°C for mercury)
Changes to boundary conditions

proton energy and beam profile

- higher proton energy \(\Rightarrow\) reduced power density in the front part
- \(\Rightarrow\) increased power density in the rear part

Power density along the beam axis for Hg with 1.334 GeV protons and LBE with 2.5 GeV protons, both for 2.3 MW heat deposition
Changes to boundary conditions

- proton energy and beam profile

- Gaussian beam profile with ± κσ·σ within the beam footprint
  ⇒ peak power density will be increased by κσ²/4

⇒ energy outside of elliptical beam footprint: $e^{-0.5\cdot\kappa^2\sigma^2}$ of total thermal energy
(has to be removed by collimator)

**Graphs:**

- **Left:** Radial distribution of rel. power density for different Gaussian profiles
- **Right:** Rel. peak power density and heat loss for different Gaussian Profiles

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Changes to boundary conditions

- pulse frequency

- decreased pulse frequency will increase the energy per pulse and therefore the temperature increment per pulse in the structure and fluid

- maximum values for a Gaussian beam profile and $κ_σ=2$

\[
\Delta T_{\text{window, 50 Hz}} \approx 6 \text{ K / pulse}
\]

\[
\Delta T_{\text{window, 16 2/3 Hz}} \approx 18 \text{ K / pulse}
\]

\[
\Delta T_{\text{LBE, 50 Hz}} \approx 26 \text{ K / pulse}
\]

\[
\Delta T_{\text{LBE, 16 2/3 Hz}} \approx 79 \text{ K / pulse}
\]
Changes to boundary conditions

- short pulse (1.4 µs) ⇒ long pulse (2 ms)

- for the long pulse target the risk of cavitation damage is significantly reduced compared to the short pulse target

- completely compressed thermal expansion of fluid
- pressure pulse only depends on total energy per pulse and not on the pulse length

- sudden change in heating rate will cause a pressure pulse at the beginning (positive) and the end (negative) of each proton pulse
- pressure pulse strongly depends on pulse length
Main concept of the ‘focused cross flow design’:
- cross flow design for same container geometry than 2003 reference target
- inclined horizontal plates accelerate the flow in the horizontal midplane
- flow pattern in the critical zones is adjusted by curvature and variable spacing of baffles (in order to generate a certain pressure drop for each ‘channel’)

outlet duct

inlet duct

inclined plates to focus the flow to the mid-plane
Focused Cross Flow Target

- total thermal power: 2.3 MW (FLUKA calculation by E. Noah)
- pulse length: 2 ms
- pulse frequency: $16\frac{2}{3}$ Hz
- mass flow rate: 155 kg/s
- $T_{\text{inlet}} = 200 \, ^\circ\text{C}$

**left:** power density for LBE during pulse in $\text{W/m}^3$

$6 \cdot 10^{10} \, \text{W/m}^3$

**right:** assumed power density for steel during pulse in $\text{W/m}^3$ (scaled by density)

$3.444 \cdot 10^{10}$
Focused Cross Flow Target

- **pros and cons**

- additional structural material within the zone of high heat deposition

*left: power density in structural material for the focused cross flow target*

*right: power density in structural material for the 2003 target design*
Focused Cross Flow Target

 pros and cons

 window cooling inferior to 2003 reference design

left: structural temperatures for focused cross flow target

right: structural temperatures for the 2003 target design

407°C + (18°C after pulse)
max. interface temperature: 351°C (+18°C)

325°C
Focused Cross Flow Target

**pros and cons**

- more reliable flow pattern and consequently more reliable heat removal
- less temperature fluctuations close to the container walls

**left:** fluid temperatures for focused cross flow target

**right:** fluid temperatures for the 2003 target design
Focused Cross Flow Target

**pros and cons**

- more reliable flow pattern and consequently more reliable heat removal
- less temperature fluctuations close to the walls

*fluid temperatures for focused cross flow target*
Focused Cross Flow Target

**pros and cons**

- reduced velocities at target window
  - less erosion problems

left: fluid velocity for focused cross flow target
right: fluid velocity for the 2003 target design

3 m/s

7.5 m/s

~5 m/s

corrosion problems at thin target window?
Focused Cross Flow Target

- **pros** and cons

- significantly reduced pressure drop
  - permitting higher flow rates

[left: absolute pressure; pressure drop: $\Delta p \approx 0.3$ bar]  
[right: absolute pressure; pressure drop: $\Delta p \approx 1.9$ bar]
Preliminary Conclusions & Outlook

- The focused cross flow target has still some potential for optimization with respect to window cooling and heat removal capability (e.g. baffle arrangement, increased mass flow rate)
- Window cooling and heat removal in the zone of maximum power density seems to be already sufficient for a 5MW proton beam

Outlook

- Temperature and velocity limits have to be defined for the target
- Further optimization of flow field
- Evaluation of thermal and mechanical stresses in the target (e.g. stresses due to pulsed operation, possible thermal striping, …)
- Producibility aspects have to be clarified
Changes to boundary conditions

LBE as preferred liquid metal

LBE as preferred target material for a liquid metal target

⇒ same pressure drop can be expected for a mass flow rate of

\[ \dot{m}_{LBE} = \dot{m}_{Hg} \sqrt{\frac{\rho_{LBE}}{\rho_{Hg}}} = 155 \frac{kg}{s} \]

(effect of viscosity neglected)

⇒ heat removal capability is comparable:

\[ \frac{\dot{m}_{LBE} \cdot c_{pLBE}}{\dot{m}_{Hg} \cdot c_{pHg}} = \frac{155 \frac{kg}{s} \cdot 146 \frac{J}{kg \cdot K}}{175 \frac{kg}{s} \cdot 136 \frac{J}{kg \cdot K}} = 0.95 \]
Changes to boundary conditions

LBE as preferred liquid metal

⇒ heat transfer coefficients are comparable:
(e.g. formulas for turbulent pipe flow, \(d \approx 100\)mm)

\[
\frac{\alpha_{\text{LBE}}}{\alpha_{\text{Hg}}} = \frac{\frac{(1.8 \cdot \log(\text{Re}_{\text{LBE}}) - 1.5)^2}{8} \cdot \text{Re}_{\text{LBE}} \cdot \text{Pr}_{\text{LBE}}}{1 + 12.7 \cdot \sqrt{\frac{(1.8 \cdot \log(\text{Re}_{\text{Hg}}) - 1.5)^2}{8} \cdot \text{Re}_{\text{Hg}} \cdot \text{Pr}_{\text{Hg}}}} \cdot \frac{\lambda_{\text{LBE}}}{d} = 1.084
\]

⇒ thermal-hydraulic design is similar for mercury and LBE

but

⇒ to avoid solidification of LBE, the inlet temperature must be significantly higher:
175 – 200 °C (> 125°C) for LBE instead of 100°C for mercury

⇒ no risk of evaporation (evaporation temperature of 1670 °C for LBE
instead of 357 °C for mercury)